



Annual Output of a New Solar Heat Engine

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Summary

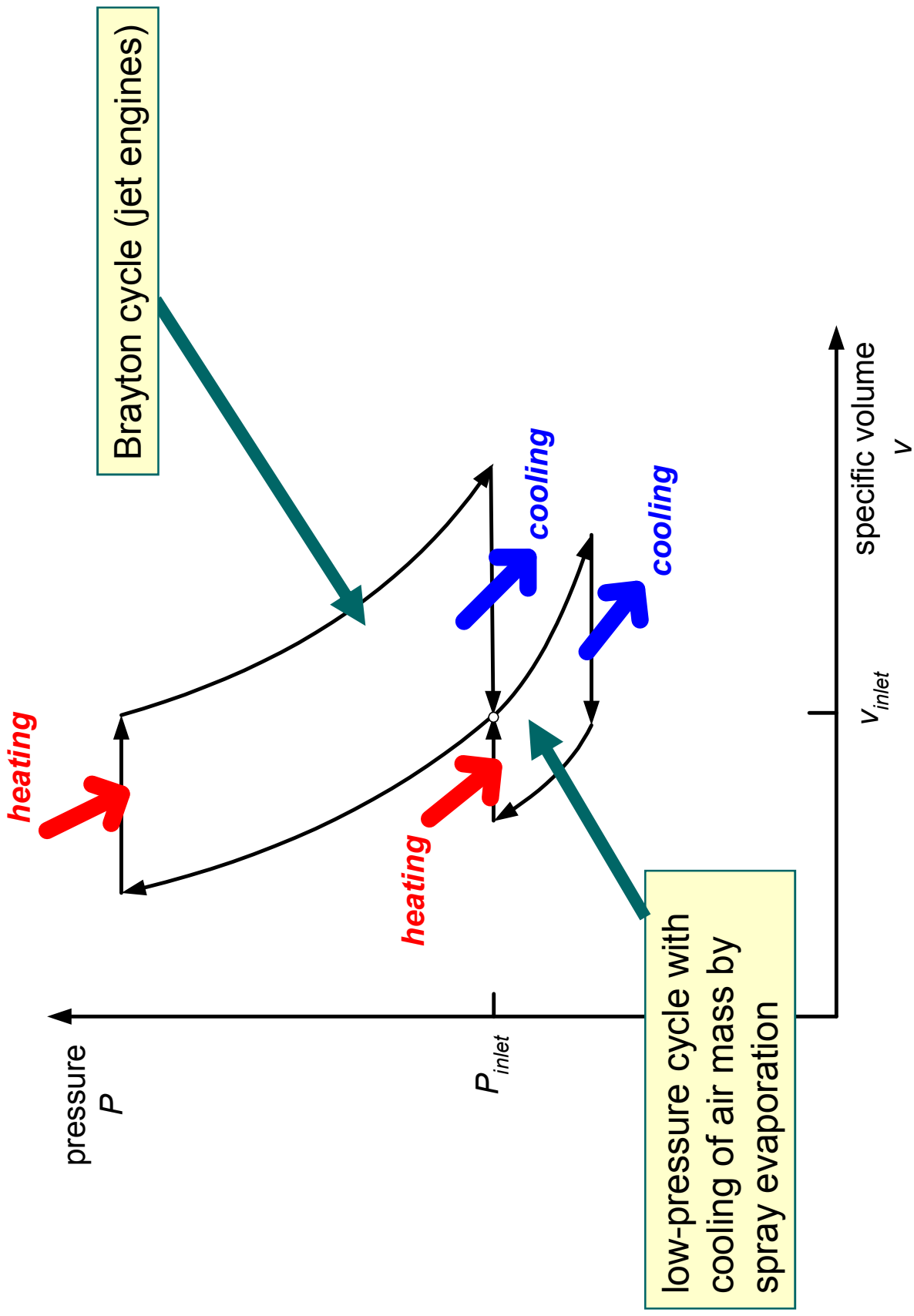
- This work involves a heat engine with a new thermodynamic cycle.
- We simulate the annual output of the engine, as powered by passive solar heat collection. Site is Wellington NSW; data from Bureau of Meteorology.
- Heat collection takes place under a transparent insulated canopy.
- The seminar describes a canopy heat transfer model coupled to a thermodynamic model of the engine. This is the basis for detailed simulations.
- Counting all losses (canopy plus engine), current estimates are:

➤ peak power	65 W/m ²	carefully estimated
➤ annual output	74 kWhr/m ²	
➤ cost per peak Watt	AUD1.38/W _p	preliminary estimate
➤ Levelised Energy Cost	AUD163/MWhr	

Contents

- Summary
- **Evaporation heat engines – quick overview**
- Canopy heat transfer model
- Numerical methods
- Results
- Losses
- Conclusions

Thermodynamic cycle (continuous-flow version)



Mechanical principle

- inlet to receive hot dry air
- expand so that pressure is reduced (but not as far as saturation by water vapour in the air)
- spray water into low-pressure section; evaporation causes a decrease in temperature AND { pressure OR specific volume }
- re-compress allowing further evaporation; there will be surplus work that can be captured by a turbine or piston
- exhaust air is cooled and moistened

water + hot dry air → power + cool moist air

evaporative coolers can also produce power!

Pressure/volume plot (evaporative cooler)

expansion ratio $r = 1.2$

inlet conditions

$$P_{air} = 99,300 \text{ Pa}$$

$$P_{vap} = 2,000 \text{ Pa}$$

$$T = 45^\circ\text{C}$$

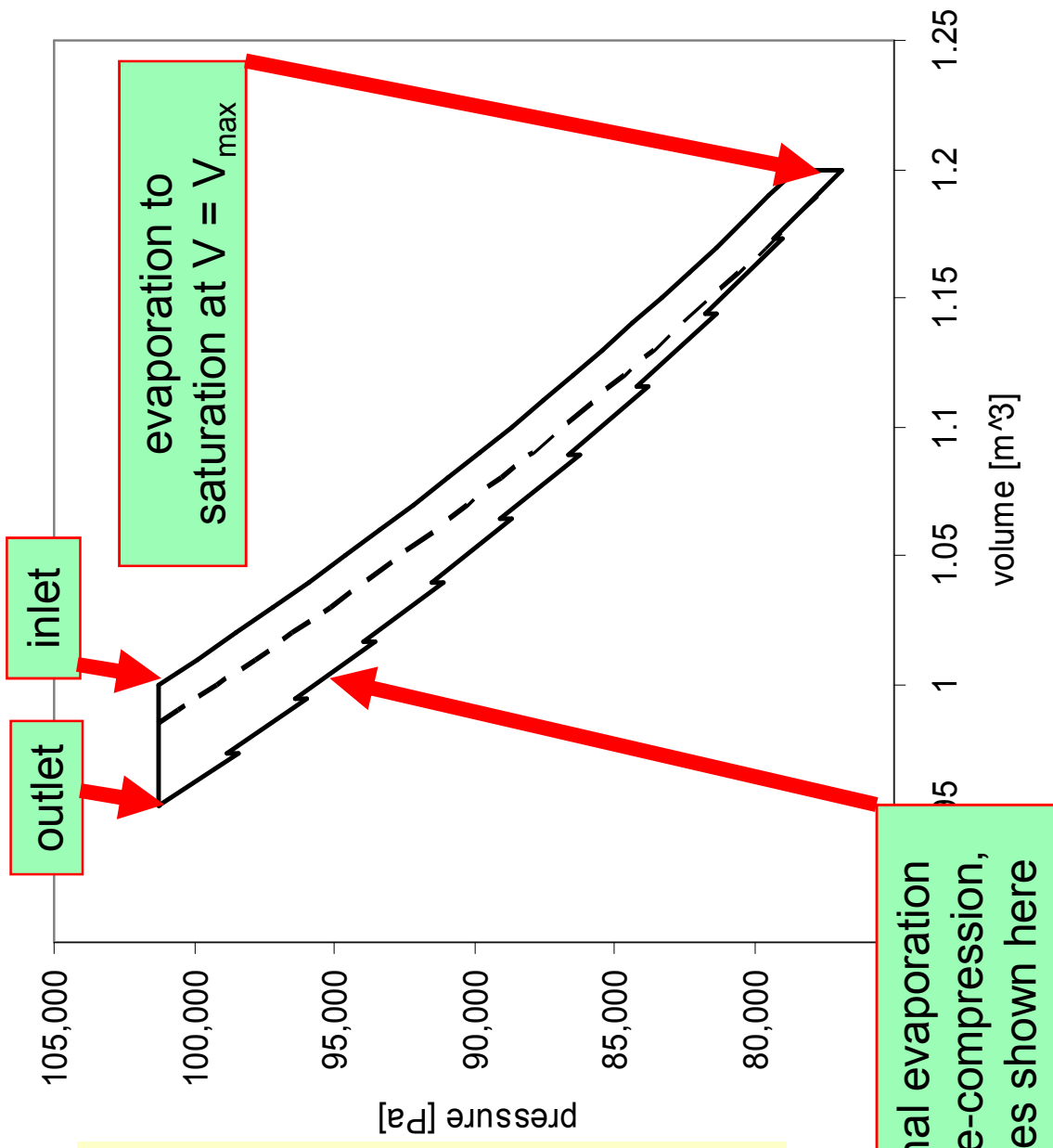
outlet conditions

$$P_{air} = 98,092 \text{ Pa}$$

$$P_{vap} = 3,208 \text{ Pa}$$

$$T = 25.5^\circ\text{C}$$

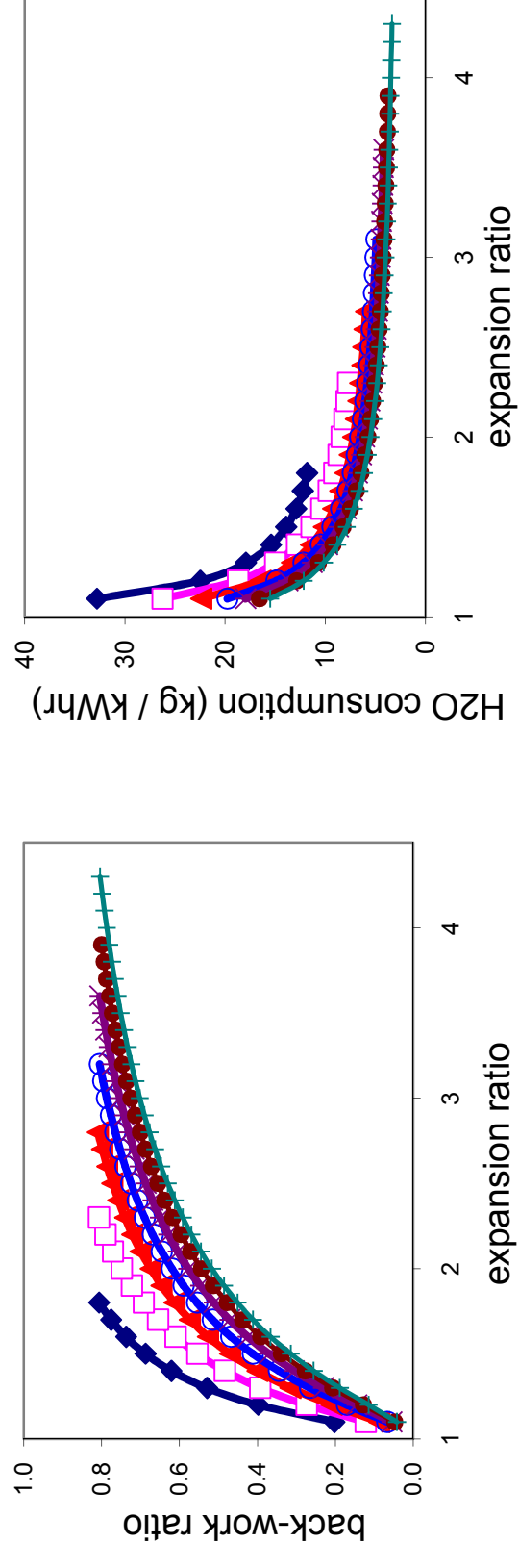
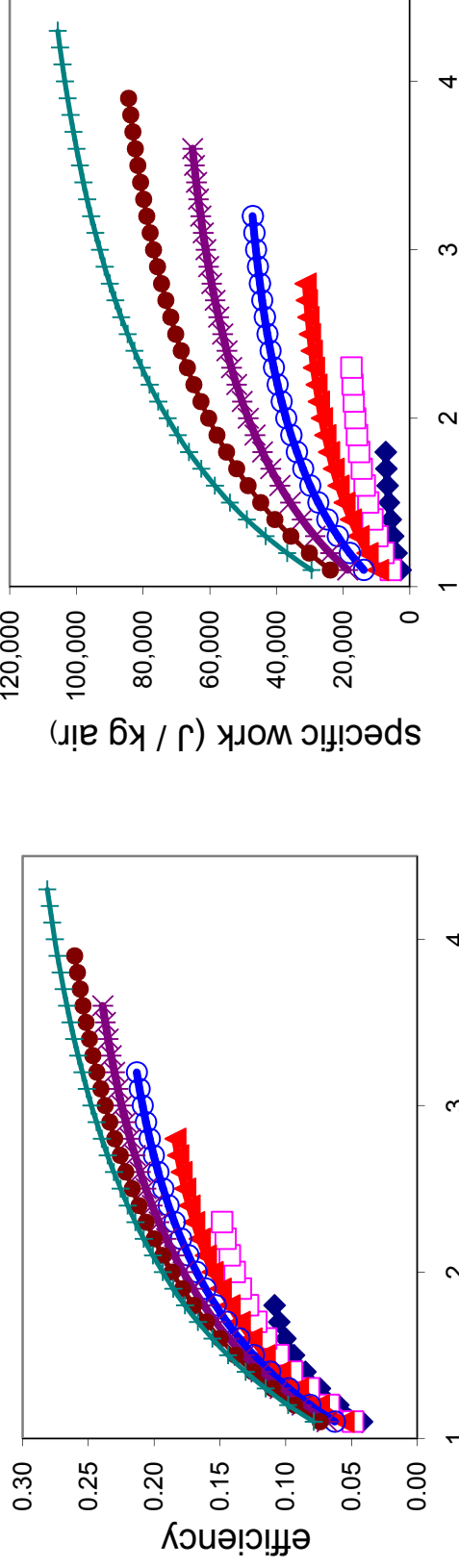
nett work per cycle
+ 788 J/kg



Theoretical analysis (piston-in-cylinder version)

- air and vapour – ideal gases with constant specific heat capacities
- isentropic expansion of air-vapour mixture
- evaporation to saturation at reduced pressure and constant volume
- re-compression of air-vapour-droplet mixture with further evaporation
- saturation given by Clausius-Clapeyron equation
- coupled algebraic equations for V , T , P_{air} , P_{vapour} , ρ_{air} , ρ_{vapour}
- Reference: N.G. Barton, “An Evaporation Heat Engine and Condensation Heat Pump”, *ANZIAM Journal*, vol 49 (2008), 503-524

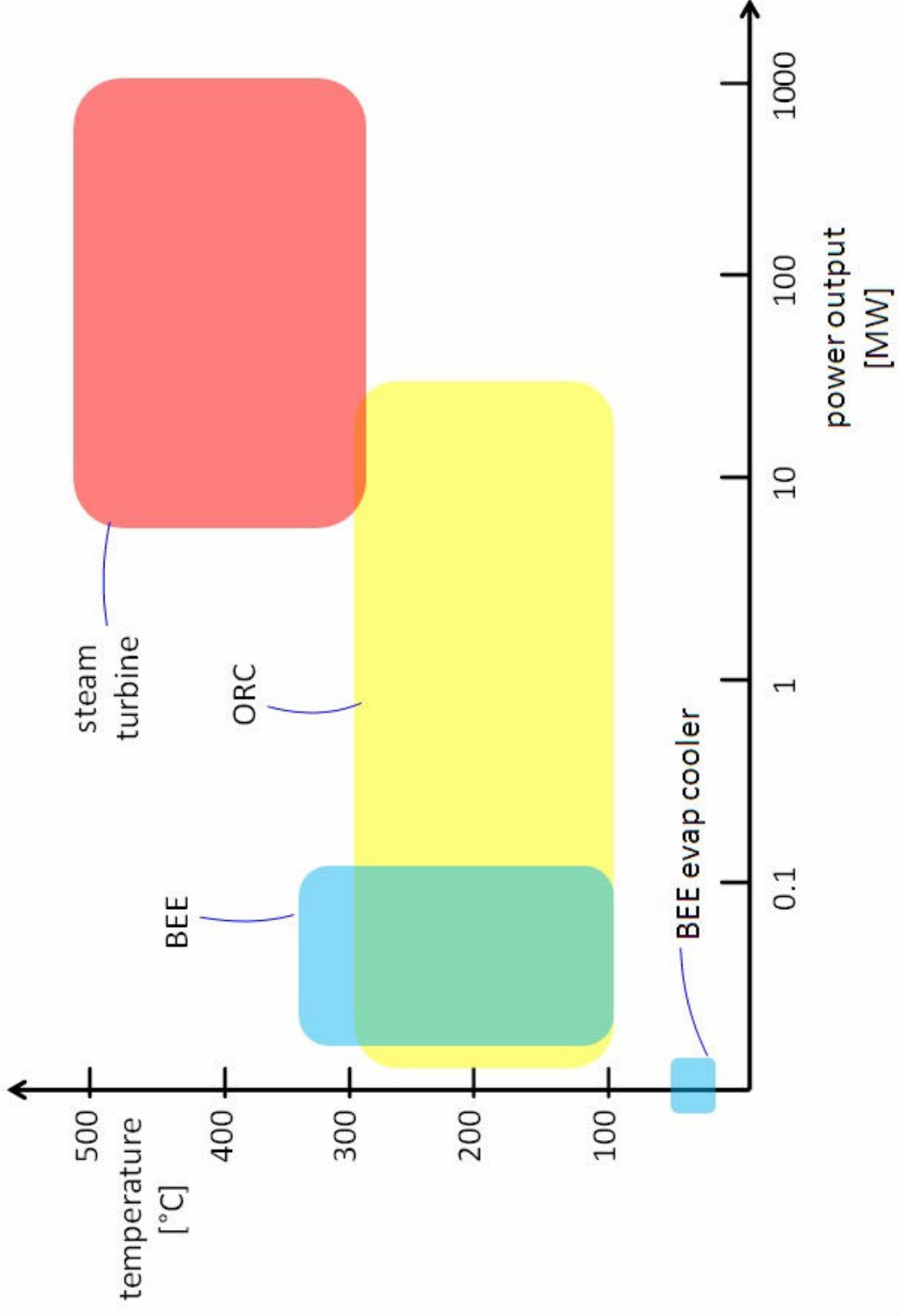
Efficiency, specific work, back-work ratio, water consumption



Ambient conditions: $P_a = 99,300 \text{ Pa}$, $P_v = 2,000 \text{ Pa}$, $T = 30^\circ\text{C}$, $T_{\text{water}} = 20^\circ\text{C}$.

Inlet temperatures: 100, 150, 200, 250, 300, 350, 400°C

Applications as an evaporative cooler and heat engine



Contents

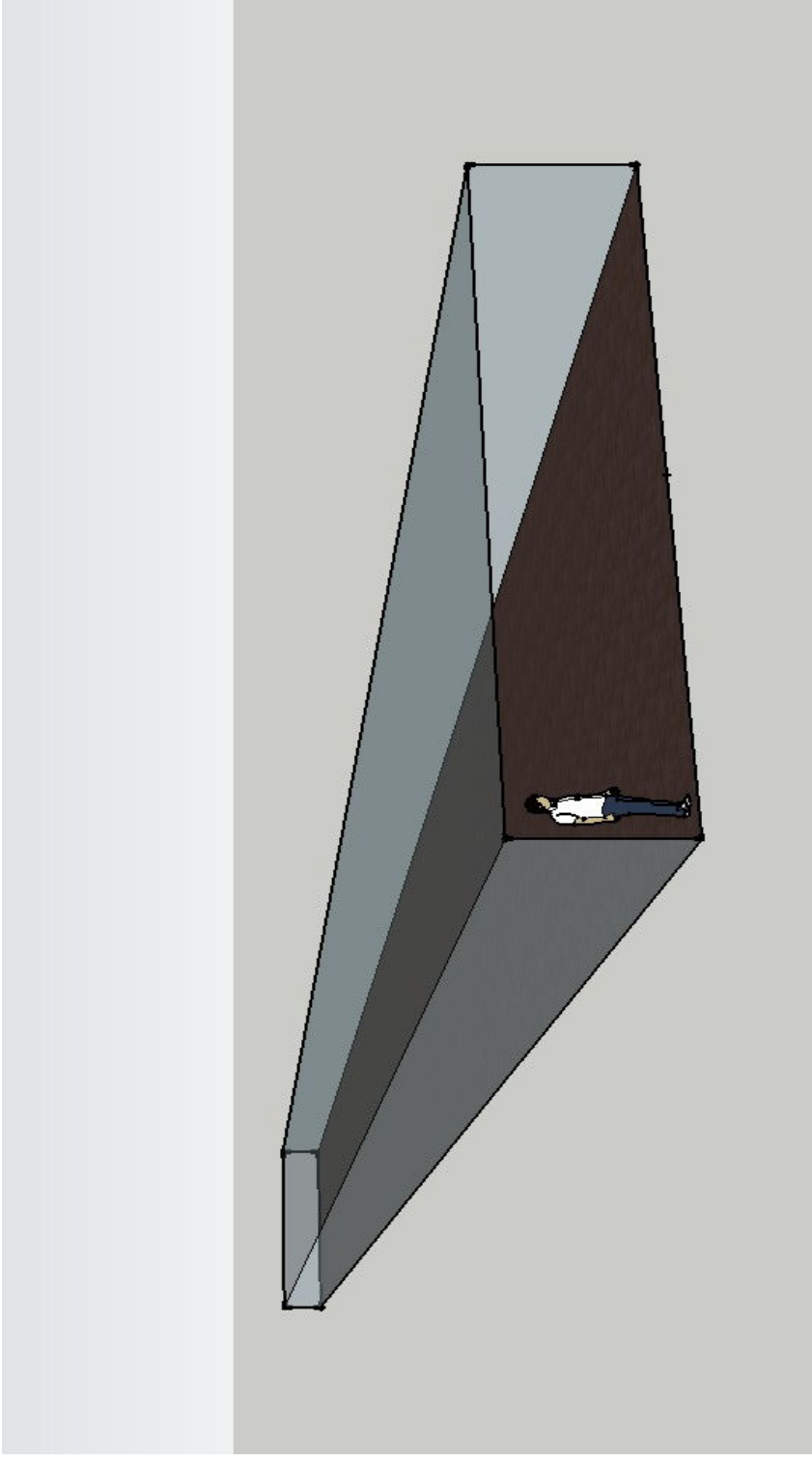
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Passive solar collectors (1)



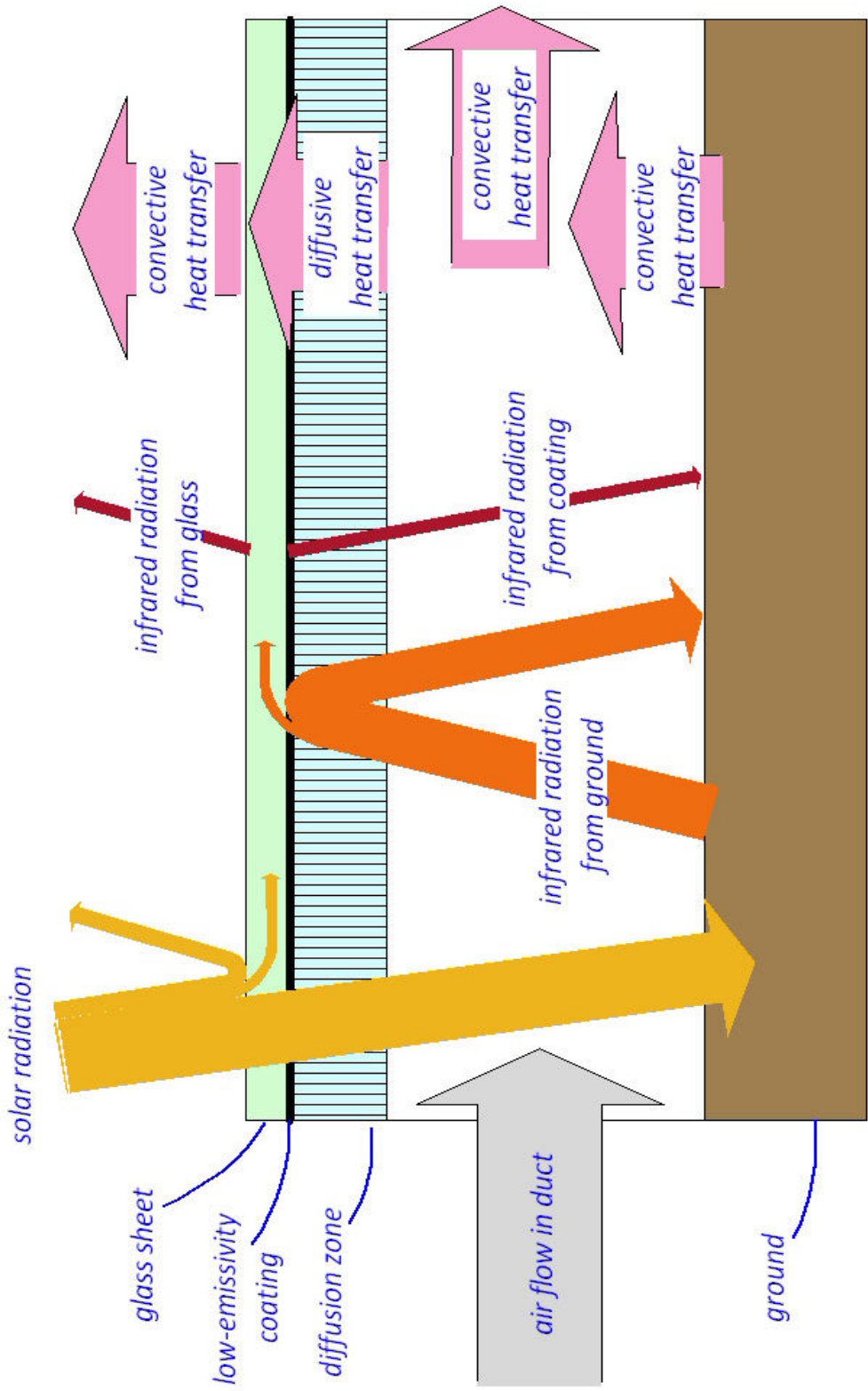
- typical commercial model shown (water-glycol coolant)
- stagnation temperature 209°C
- at 1 kW direct insolation, peak power is $827 \text{ W}_{\text{th}}/\text{m}^2$ (when storage temperature = ambient)
- used for hot water, space heating, process heat

Passive solar collectors (2)



- air is drawn by the engine through a 'glasshouse'
- canopy has low-emissivity coating and is insulated
- simulations based on 1,000 m² canopy (100 m × 10 m × 2 m)

Elements of the heat transfer model



Equations (1)

1D steady-state heat transfer in the duct under the canopy:

$$\Phi C_{aP} \frac{dT_a}{dx} = F_s + F_{ir,c2} + F_{ir,g} + F_c$$

$$T_a(0) = T_0$$

inlet condition

$$\Phi = HWU\rho_a$$

mass flux

$$F_s = W \cdot \tau_{s,c}(\theta) I_s \sin \theta$$

gain (incident solar radiation)

$$F_{ir,c2} = W \cdot I_{ir,c2}$$

gain (infrared from cover)

$$F_{ir,g} = -W \cdot (1 - \beta_{ir,c2}) I_{ir,g}$$

loss (infrared from ground)

$$F_c = - (Wk_a/d) \cdot (T_a - T_{c2})$$

loss (diffusion zone)

Equations (2)

Heat diffusion through the glass cover:

$$\begin{aligned} k_c \frac{d^2 T_c}{dz^2} &= -\frac{1}{e} \left\{ \alpha_{s,c} I_s \cdot \sin \theta + \alpha_{ir,c} I_{ir,g} \right\} \\ - \left[k_c \frac{\partial T_c}{\partial z} \right]_{z=H} &= \frac{k_a}{d} (T_a - T_{c2}) - I_{ir,c2} \quad \text{bottom surface} \\ - \left[k_c \frac{\partial T_c}{\partial z} \right]_{z=H+e} &= h_{c/o} (T_{c1} - T_o) + I_{ir,c1} \quad \text{top surface} \end{aligned}$$

Infrared radiation terms take the form:

$$I = \alpha \sigma T^4$$

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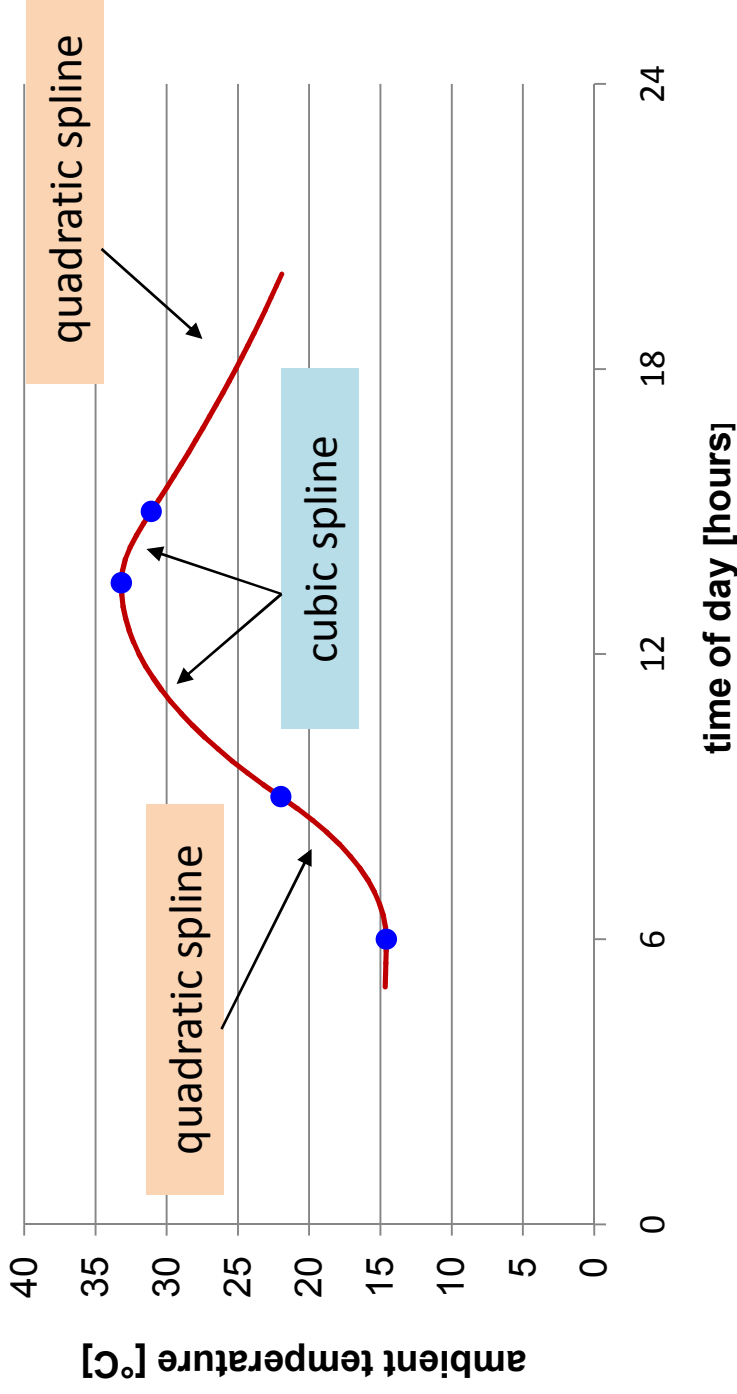
Numerical techniques

- calculate I_s ,

$$\int_{\text{dawn}}^{\text{dusk}} I_s \sin \theta(t) dt = I_s \cdot \int_{\text{dawn}}^{\text{dusk}} \sin \theta(t) dt = \text{daily insolation}$$

- sun angle from www.sunposition.info; assign other parameters
- heat transfer models for air and glass need to be solved jointly
- predictor-corrector method used; involves analytical solution in glass cover
- key factor is air mass flow-rate $\Phi = HWU\rho_a$
- flow-rate increases, then
 - temperature decreases
 - efficiency decreases but losses also decrease
- optimum flow-rate during each time interval found by simple root-finding procedure

Ambient temperature on a typical day (1 November 2009)



- BoM data for 0900 and 1500 hours, maximum and minimum
- min/max assigned to 0500/1230 (with daylight saving adjustment)

Pilkington data on transmission and reflection

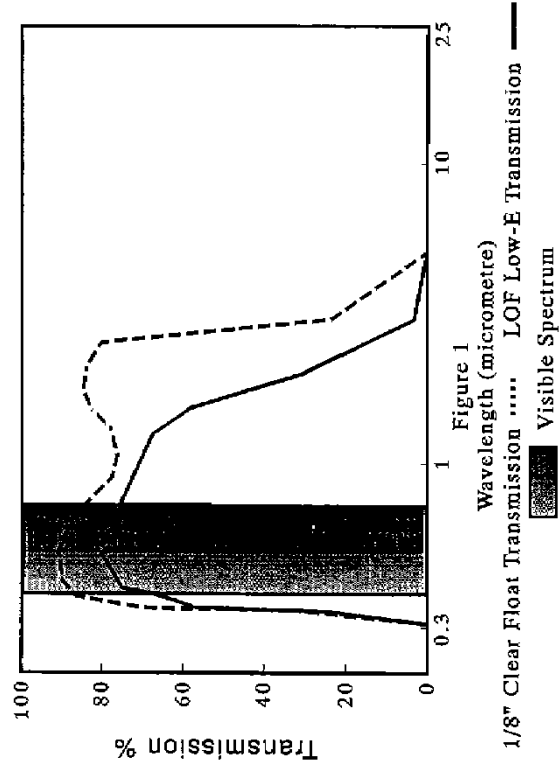


Figure 1
Wavelength (micrometre)
1/8" Clear Float Transmission LOF Low-E Transmission
Visible Spectrum

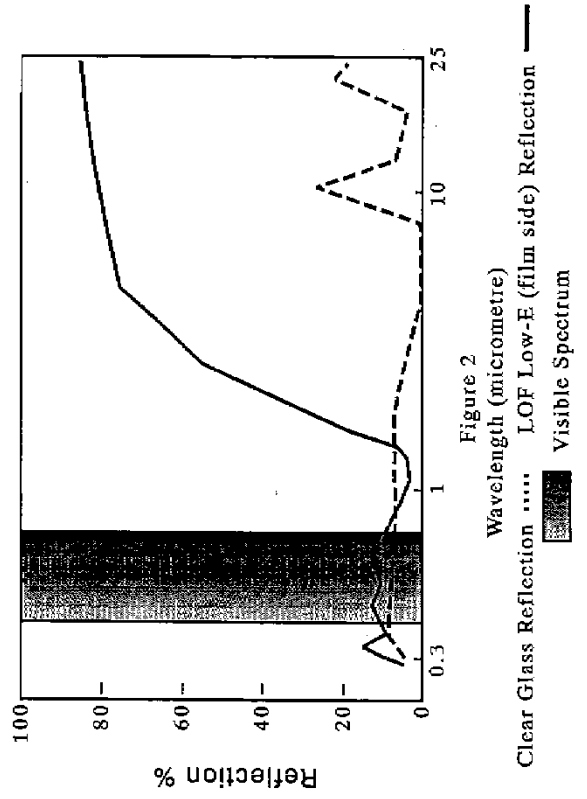
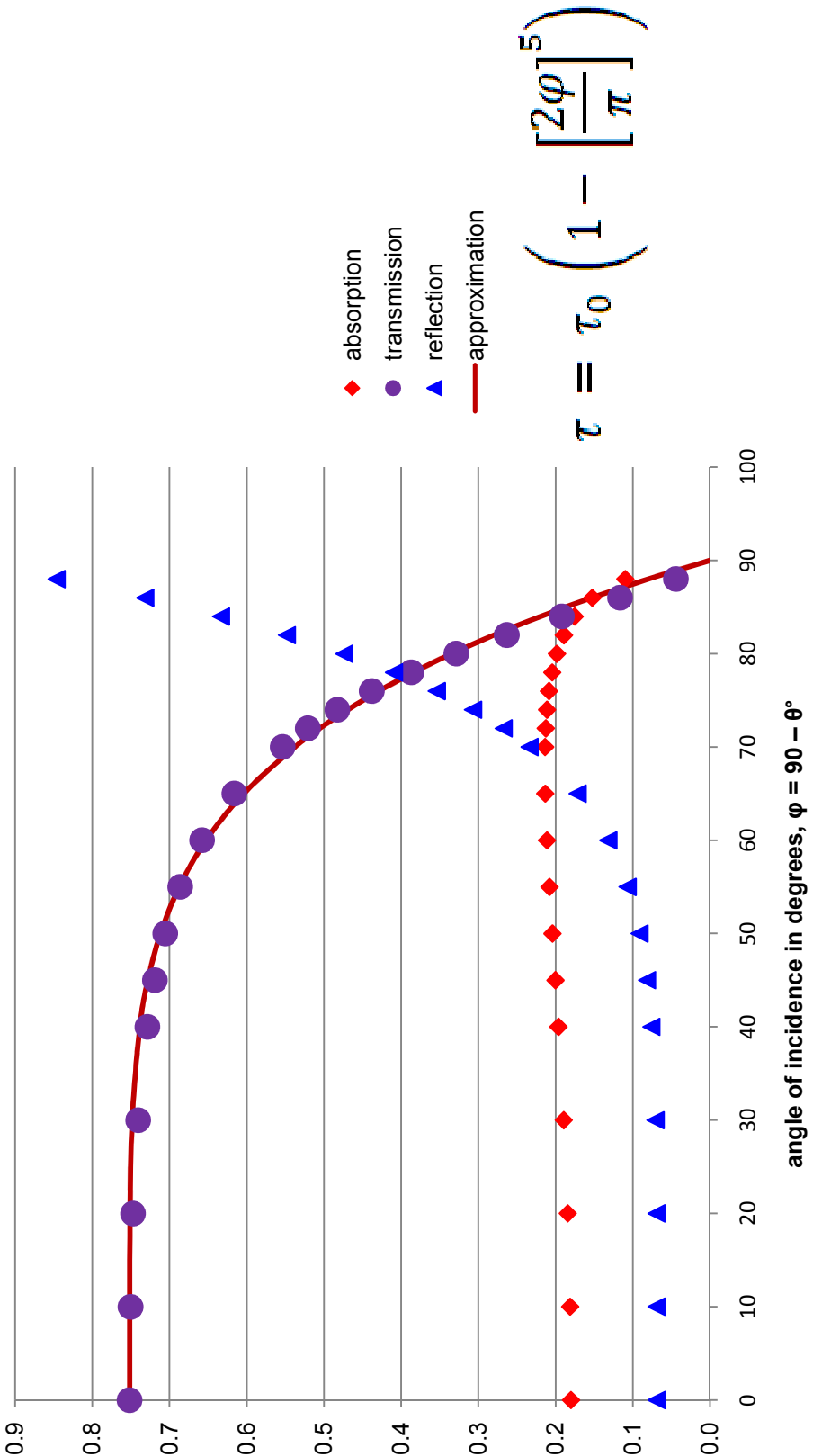


Figure 2
Wavelength (micrometre)
Clear Glass Reflection LOF Low-E (film side) Reflection
Visible Spectrum

Incident angle modifier (from Mitalas & Stephenson, 1962)



Other data

L	100 m	$\alpha_{s,c}$	0.18	C_{aP}	$1,005 \text{ J} \cdot (\text{kg} \cdot \text{K})^{-1}$
W	10 m	$\beta_{s,c}$	0.12 *	C_{aV}	$718 \text{ J} \cdot (\text{kg} \cdot \text{K})^{-1}$
H	2 m	$\alpha_{ir,c}$	0.15	C_{vP}	$1,872 \text{ J} \cdot (\text{kg} \cdot \text{K})^{-1}$
d	0.025 m	$\beta_{ir,c}$	0.85	C_{vV}	$1,411 \text{ J} \cdot (\text{kg} \cdot \text{K})^{-1}$
e	0.003 m	ρ_c	$2,500 \text{ kg} \cdot \text{m}^{-3}$	k_a	$0.0261 \text{ J} \cdot (\text{kg} \cdot \text{K})^{-1}$
δx	2 m	k_c	$1.20 \text{ W} \cdot (\text{m} \cdot \text{K})^{-1}$	$h_{c/o}$	$50 \text{ W} \cdot (\text{m}^2 \cdot \text{K})^{-1}$
r	1.9	C_c	$840 \text{ J} \cdot (\text{kg} \cdot \text{K})^{-1}$	σ	$5.67 \times 10^{-8} \text{ W} \cdot (\text{m}^2 \cdot \text{K}^4)^{-1}$

- vapour pressure average of 0900 and 1500 readings
- air pressure 97,630 Pa (Wellington is 305 m above sea level)
- canopy model assumes dry air; thermodynamic model includes water vapour
- air and vapour treated as ideal gases with constant specific heats

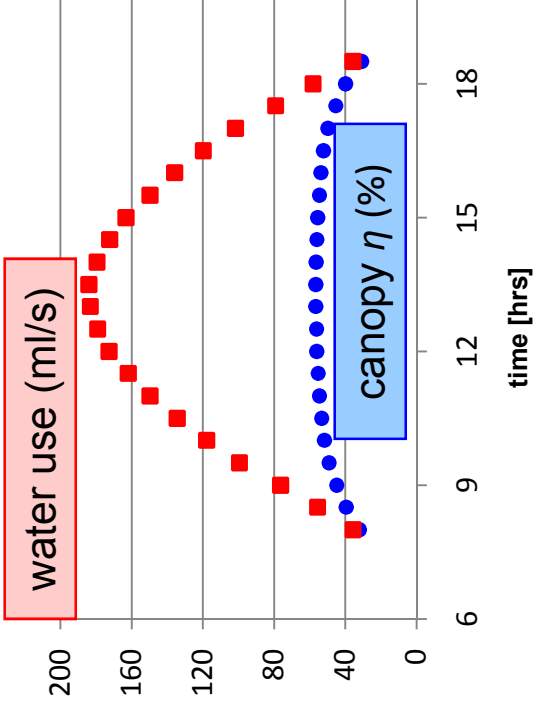
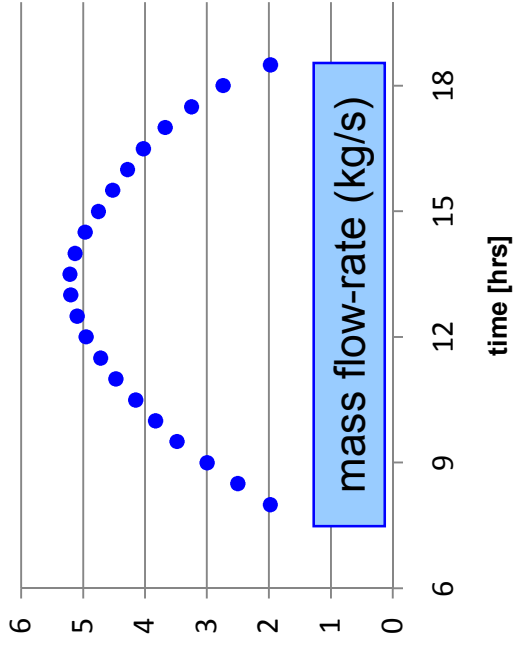
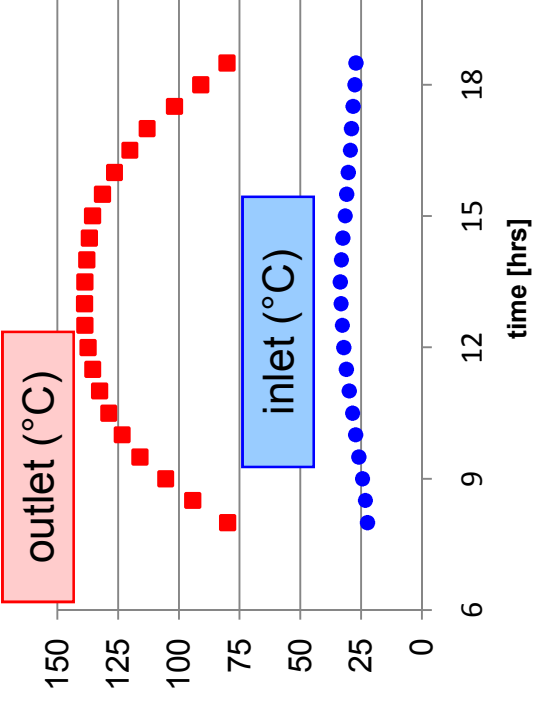
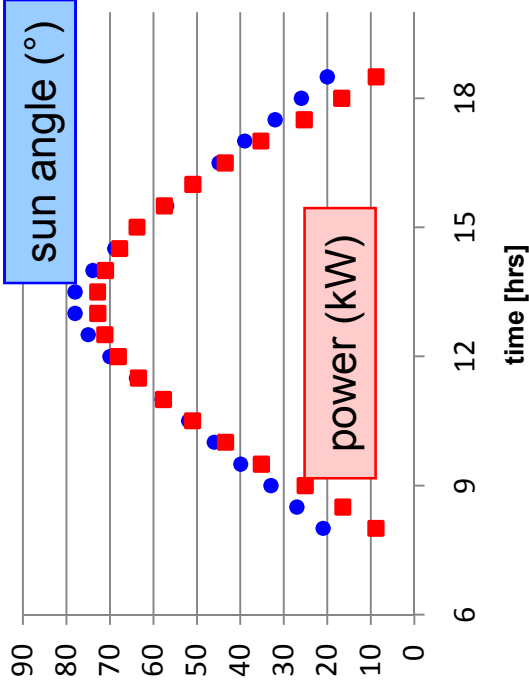
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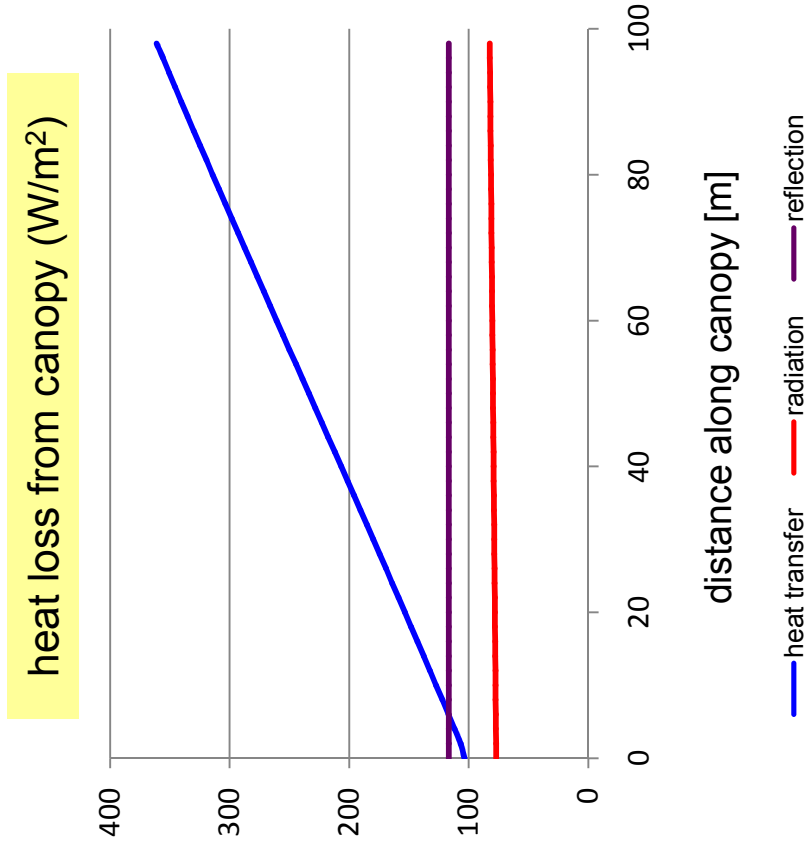
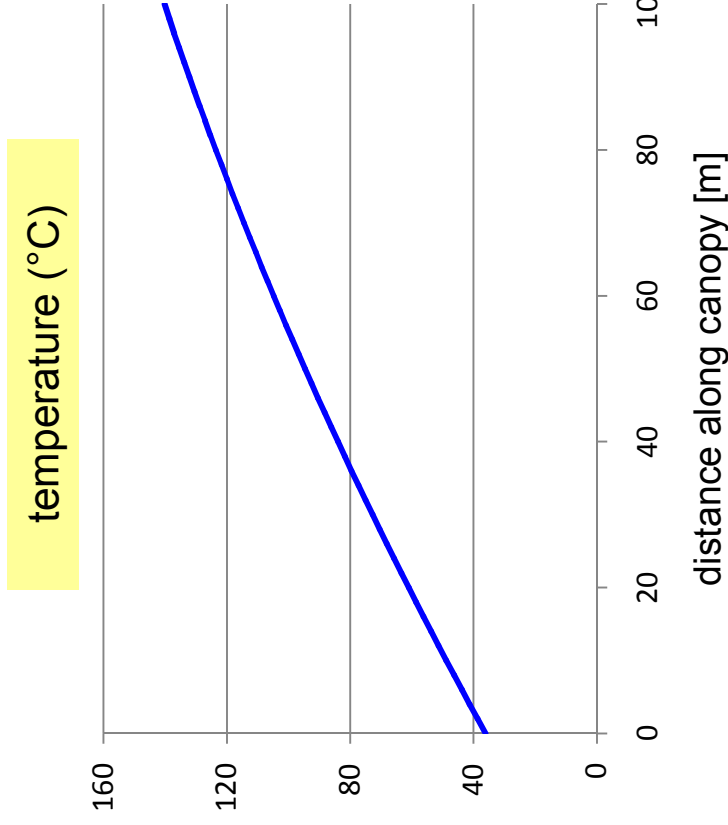
Results for a typical summer day (15 January 2010)

- lovely day for solar energy, although humid for Wellington in summer
- 30.5 MJ/m² insolation; 11 hours of sunshine; $I_s = 995 \text{ W/m}^2$
- temperatures:
 - 0900 24.5°C
 - maximum 33.5°C
 - 1500 31.6°C
- average vapour pressure 1,920 Pa (63% RH at 0900, 41% at 1500)

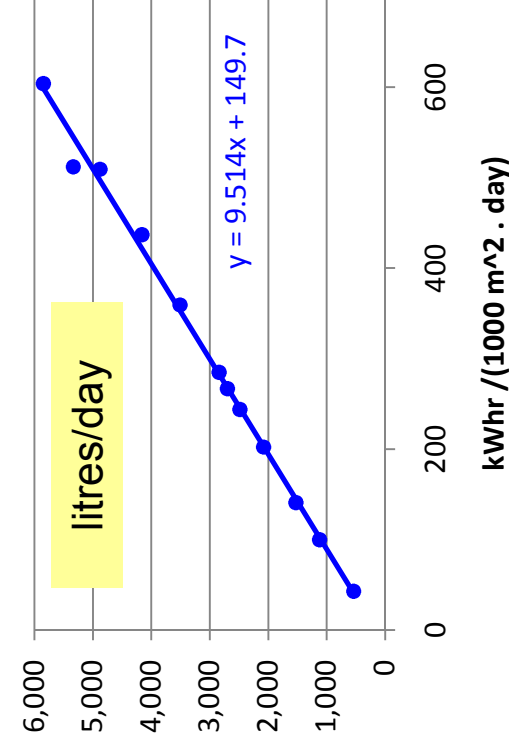
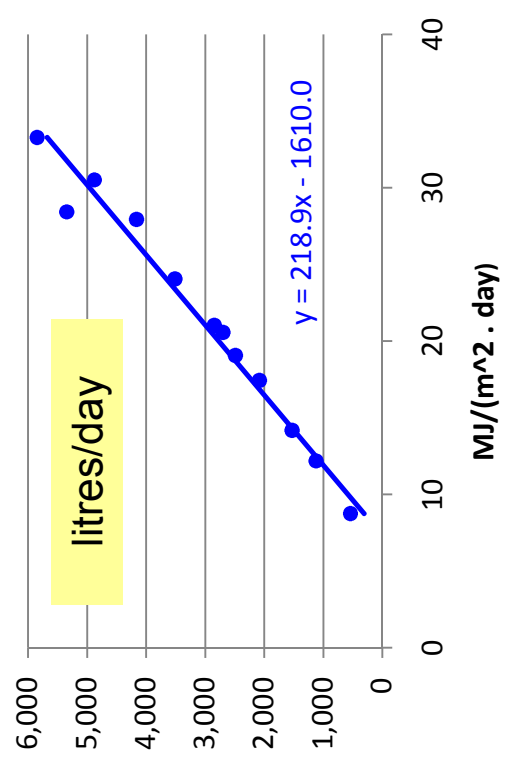
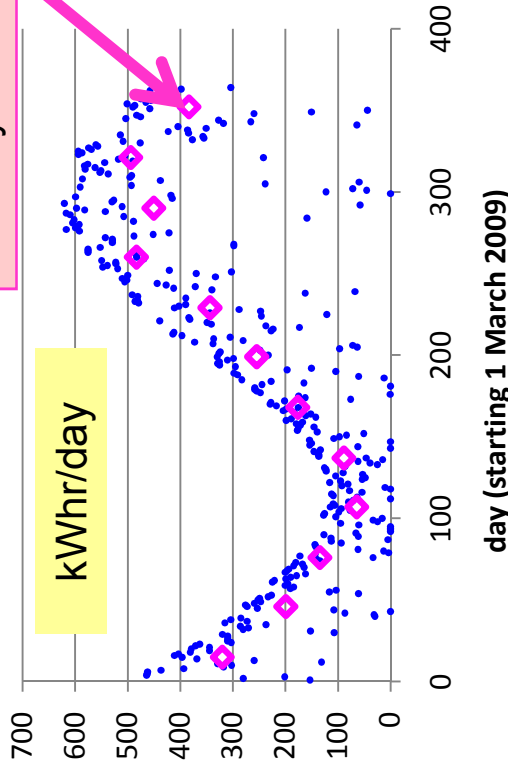
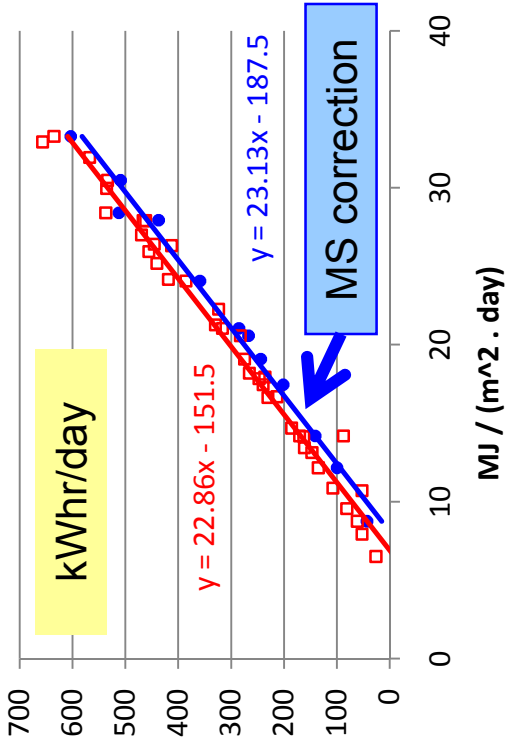
Results for 15 January 2010 (for 1,000 m² canopy, no engine losses)



15 January 2010 at 1330 hours



Annual results for 1,000 m² canopy (no engine losses)



Annual results from Wellington simulations

Power output: 104 MWhr / (1,000 m².yr)

Water consumption: 1,038 m³ / (1,000 m².yr)

(considering canopy losses but not engine losses)

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Engine losses

- transient heat transfer 7%
- leakage around valves and seals 1%
- dead zones 1%
- incomplete evaporation during re-compression 4%
- aerodynamic valve losses 1%
- mechanical friction 4%
- RO water purification 0.004 MWhr/m³
- water injection 0.0028 MWhr/m³
- mechanical/electrical conversion 3%

Estimates

- engine losses lead to 25-30% reduction in simulated power output
- water consumption 14% higher than theoretical estimate

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Estimates of costs for a 1,000 m² canopy, 65 kW engine, 74 MWhr/year

Basis for estimates: mass-produced components, operated as part of a big system at location like Wellington

Caution: estimates are preliminary, taxation not considered

Cost of land, earthworks, frame and glass	\$25/m ² , so \$25,000 per canopy
Cost of engine and balance of plant	\$1,000/kW, so \$65,000 for a 65 kW engine
Capital cost	\$90,000
Interest rate	8%
Rate of capital return (based on 8% interest and 25 year pay-back)	9.368%
Capital expenditure per year	$0.09368 \times 90,000 = \$8,431$
Operating expenditure per year	4% of capital cost, hence \$3,600
Expenditure per year	$\$8,431 + \$3,600 = \$12,031$
Metric 1: cost per peak Watt	$\\$90,000/65,000W = \\$1.38/W_p$
Metric 2: Levelised Energy Cost	$\\$12,031/74 = \\$163/MWhr$

Final remarks

- Simulations provide a basis to estimate performance.
- Maximum temperature $\approx 140^{\circ}\text{C}$; some engine components can be plastic.
- Engine will be large, multi-cylinder, lightly stressed, slow-revving.
- Heat exchangers and condensers not required.
- Engine does not require sophisticated manufacturing techniques (*cf* PV).
- Canopy run-off in Wellington would meet 58% of water need.
- Further studies: sloping canopy, true desert location, variable r .
- Construction of a prototype would greatly increase the knowledge base.
- Investors are needed for further progress.